



## Navier-Stokes Equations

### 3 - dimensional - unsteady

Glenn  
Research  
Center

Continuity:

$$\frac{\partial \rho}{\partial t} + \frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} + \frac{\partial(\rho w)}{\partial z} = 0$$

X - Momentum:

$$\frac{\partial(\rho u)}{\partial t} + \frac{\partial(\rho u^2)}{\partial x} + \frac{\partial(\rho uv)}{\partial y} + \frac{\partial(\rho uw)}{\partial z} = -\frac{\partial p}{\partial x} + \frac{1}{Re_r} \left[ \frac{\partial \tau_{xx}}{\partial x} + \frac{\partial \tau_{xy}}{\partial y} + \frac{\partial \tau_{xz}}{\partial z} \right]$$

Y - Momentum:

$$\frac{\partial(\rho v)}{\partial t} + \frac{\partial(\rho uv)}{\partial x} + \frac{\partial(\rho v^2)}{\partial y} + \frac{\partial(\rho vw)}{\partial z} = -\frac{\partial p}{\partial y} + \frac{1}{Re_r} \left[ \frac{\partial \tau_{xy}}{\partial x} + \frac{\partial \tau_{yy}}{\partial y} + \frac{\partial \tau_{yz}}{\partial z} \right]$$

Z - Momentum

$$\frac{\partial(\rho w)}{\partial t} + \frac{\partial(\rho uw)}{\partial x} + \frac{\partial(\rho vw)}{\partial y} + \frac{\partial(\rho w^2)}{\partial z} = -\frac{\partial p}{\partial z} + \frac{1}{Re_r} \left[ \frac{\partial \tau_{xz}}{\partial x} + \frac{\partial \tau_{yz}}{\partial y} + \frac{\partial \tau_{zz}}{\partial z} \right]$$

Energy:

$$\begin{aligned} \frac{\partial(E_T)}{\partial t} + \frac{\partial(uE_T)}{\partial x} + \frac{\partial(vE_T)}{\partial y} + \frac{\partial(wE_T)}{\partial z} = & -\frac{\partial(up)}{\partial x} - \frac{\partial(vp)}{\partial y} - \frac{\partial(wp)}{\partial z} - \frac{1}{Re_r Pr_r} \left[ \frac{\partial q_x}{\partial x} + \frac{\partial q_y}{\partial y} + \frac{\partial q_z}{\partial z} \right] \\ & + \frac{1}{Re_r} \left[ \frac{\partial}{\partial x} (u\tau_{xx} + v\tau_{xy} + w\tau_{xz}) + \frac{\partial}{\partial y} (u\tau_{xy} + v\tau_{yy} + w\tau_{yz}) + \frac{\partial}{\partial z} (u\tau_{xz} + v\tau_{yz} + w\tau_{zz}) \right] \end{aligned}$$

Time: t

Density:  $\rho$

Total Energy: Et

Reynolds Number: Re

Coordinates: (x,y,z)

Stress:  $\tau$

Heat Flux: q

Prandtl Number: Pr

Velocity Components: (u,v,w)

Pressure: p

On this slide we show the three-dimensional unsteady form of the **Navier-Stokes Equations**. These equations describe how the velocity, pressure, temperature, and density of a moving fluid are related. The equations were derived independently by G.G. Stokes, in England, and M. Navier, in France, in the early 1800's. The equations are extensions of the Euler Equations and include the effects of viscosity on the flow. These equations are very complex, yet undergraduate engineering students are taught how to derive them in a process very similar to the derivation that we present on the conservation of momentum web page.

The equations are a set of coupled **differential equations** and could, in theory, be solved for a given flow problem by using methods from **calculus**. But, in practice, these equations are too difficult to solve analytically. In the past, engineers made further approximations and simplifications to the equation set until they had a group of equations that they could solve. Recently, high speed computers have been used to solve approximations to the equations using a variety of techniques like finite difference, finite volume, finite element, and spectral methods. This area of study is called **Computational Fluid Dynamics** or **CFD**.

The Navier-Stokes equations consists of a time-dependent continuity equation for conservation of mass, three time-dependent conservation of momentum equations and a time-dependent conservation of energy equation. There are four independent variables in the problem, the x, y, and z spatial coordinates of some domain, and the time t. There are six dependent variables; the pressure p, density  $\rho$ , and temperature T (which is contained in the energy equation through the total energy Et) and three components of the velocity vector; the u component is in the x direction, the v component is in the y direction, and the w component is in the z direction. All of the dependent variables are functions of all four independent variables. The differential equations are therefore **partial** differential equations and not

## Navier-Stokes Equations

Page 2 of 3

the **ordinary** differential equations that you study in a beginning calculus class. You will notice that the differential symbol is different than the usual "d /dt" or "d /dx" that you see for ordinary differential equations. The symbol look like a backwards "6", and, because of font limitations, we will use the symbol "6 /6t" on this page to indicate partial derivatives. The symbol indicates that we are to hold all of the independent variables fixed, except the variable next to symbol, when computing a derivative. The set of equations are:

$$\text{Continuity: } 6r/6t + 6(r * u)/6x + 6(r * v)/6y + 6(r * w)/6z = 0$$

$$\begin{aligned} \text{X - Momentum: } 6(r * u)/6t + 6(r * u^2)/6x + 6(r * u * v)/6y + 6(r * u * w)/6z = & - 6p/6x \\ & + 1/Re * \{ 6\tau_{xx}/6x + 6\tau_{xy}/6y + 6\tau_{xz}/6z \} \end{aligned}$$

$$\begin{aligned} \text{Y - Momentum: } 6(r * v)/6t + 6(r * u * v)/6x + 6(r * v^2)/6y + 6(r * v * w)/6z = & - 6p/6y \\ & + 1/Re * \{ 6\tau_{xy}/6x + 6\tau_{yy}/6y + 6\tau_{yz}/6z \} \end{aligned}$$

$$\begin{aligned} \text{Z - Momentum: } 6(r * w)/6t + 6(r * u * w)/6x + 6(r * v * w)/6y + 6(r * w^2)/6z = & - 6p/6z \\ & + 1/Re * \{ 6\tau_{xz}/6x + 6\tau_{yz}/6y + 6\tau_{zz}/6z \} \end{aligned}$$

$$\begin{aligned} \text{Energy: } 6Et/6t + 6(u * Et)/6x + 6(v * Et)/6y + 6(w * Et)/6z = & - 6(r * u)/6x - 6(r * v)/6y - 6(r * w)/6z \\ & - 1/(Re*Pr) * \{ 6q_x/6x + 6q_y/6y + 6q_z/6z \} \\ & + 1/Re * \{ 6(u * \tau_{xx} + v * \tau_{xy} + w * \tau_{xz})/6x + 6(u * \tau_{xy} + v * \tau_{yy} + w * \tau_{xz})/6y + 6(u * \tau_{xz} + v * \tau_{yz} + w * \tau_{zz})/6z \} \end{aligned}$$

where Re is the Reynolds number which is a similarity parameter that is the ratio of the scaling of the inertia of the flow to the viscous forces in the flow. The **q** variables are the heat flux components and Pr is the Prandtl number which is a similarity parameter that is the ratio of the viscous stresses to the thermal stresses. The **tau** variables are components of the **stress tensor**. A tensor is generated when you multiply two vectors in a certain way. Our velocity vector has three components; the stress tensor has nine components. Each component of the stress tensor is itself a second derivative of the velocity components.

The terms on the left hand side of the momentum equations are called the **convection terms** of the equations. Convection is a physical process that occurs in a flow of gas in which some property is transported by the ordered motion of the flow. The terms on the right hand side of the momentum equations that are multiplied by the inverse Reynolds number are called the **diffusion terms**. Diffusion is a physical process that occurs in a flow of gas in which some property is transported by the random motion of the molecules of the gas. Diffusion is related to the stress tensor and to the viscosity of the gas. Turbulence, and the generation of boundary layers, are the result of diffusion in the flow. The Euler equations contain only the convection terms of the Navier-Stokes equations and can not, therefore, model boundary layers. There is a special simplification of the Navier-Stokes equations that describe boundary layer flows.

Notice that all of the dependent variables appear in each equation. To solve a flow problem, you have to solve all five equations simultaneously; that is why we call this a **coupled** system of equations. There are actually some other equation that are required to solve this system. We only show five equations for

## Navier-Stokes Equations

Page 3 of 3

six unknowns. An equation of state relates the pressure, temperature, and density of the gas. And we need to specify all of the terms of the stress tensor. In CFD the stress tensor terms are often approximated by a turbulence model.

---

Activities:[Show Slide](#)

---

Guided Tours

---

Navigation ..[Aerodynamics Index](#)[Propulsion Index](#)[Beginner's Guide Home Page](#)[NASA Glenn Learning Technologies Home Page](#)<http://www.grc.nasa.gov/WWW/K-12>

---

*by Tom Benson**Please send suggestions/corrections to: [Thomas.J.Benson@nasa.gov](mailto:Thomas.J.Benson@nasa.gov)**Last Updated Wed, Apr 14 03:55:22 PM EDT 2004 by Tom Benson*

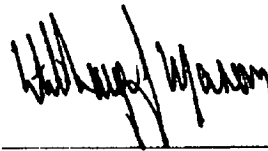
IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

Honorable Director of Patents and Trademarks  
Alexandria, VA 22313  
Sir:

CERTIFICATE OF TRANSMISSION

Date of Deposit: June 10, 2004

I hereby certify that this paper, which is an Amendment for the TURBULENCE-FREE LABORATORY SAFETY ENCLOSURE (DIV) S/N 10/690379 is being sent via facsimile 703-872-9306 to the United States Patent and Trademark Office on the date indicated above.



---

William J. Mason  
Registration No. 22,948

Our File No.: 5011-016A